

# Power-and-Biogas-to-Liquid Power-and-Gas-to-Liquid

# **PBtL / PGtL**

**7. Central European Biomass Conference 2023** Kay Kratky, Chair of Caphenia Adv. Board



## 10 years R&D

### **Private Investment > 10 mio EUR**

## First Plant start Construction Components Q2 2023

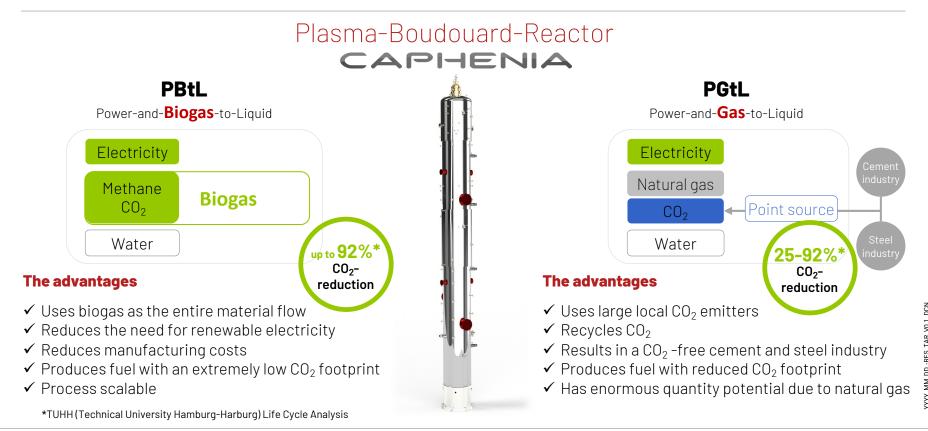
A unique, new technology route for synthesis gas production:

Power-and-Biogas-to-LiquidPBtLPower-and-Gas-to-LiquidPGtL

# **CAPHENIA : One Technology. Two Applications.**

Option 1: genetically green.

Option 2: almost unlimited feedstock.



### The Task: Convert Methane & CO<sub>2</sub> to Syn Gas to Fuels

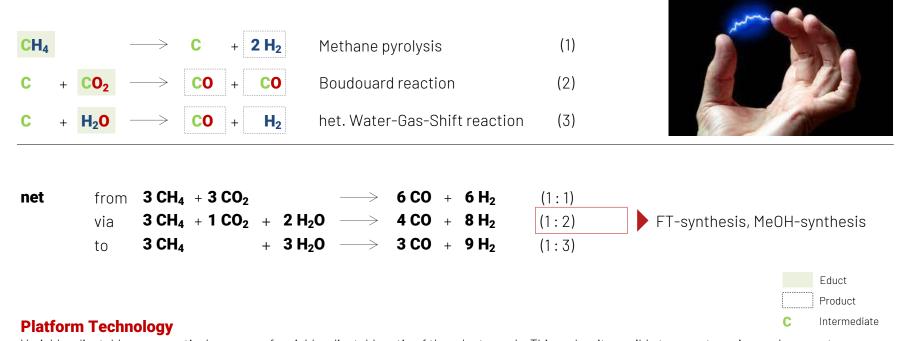
The Core Component: Caphenia's Plasma Boudouard Reactor (PBR)

A unique, efficient and sustainable process for the production of synthesis gas (Syngas)



### Three well-known chemical reactions, which have never been combined before

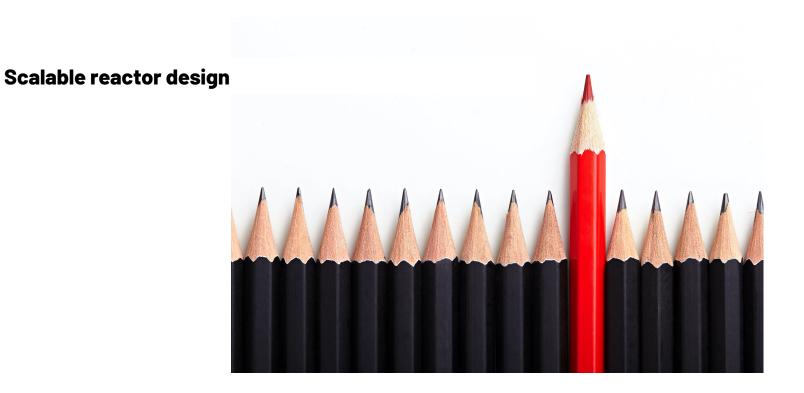
The CAPHENIA process: A unique, new route for the production of variable synthesis gas



Variably adjustable syngas ratio, by means of variably adjustable ratio of the educt supply. This makes it possible to operate various subsequent synthesis steps. CAPHENIA's platform technology is suitable for the production of fuels and basic chemicals. Optimum Case refering to a biogas structure CH4/C02 by 70-75/25-30%

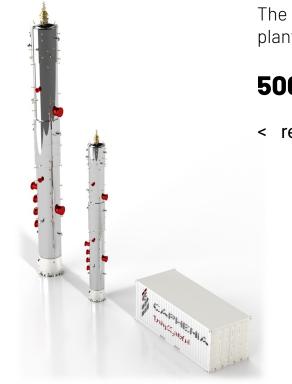
### **Biogas Plants and CAPHENIA's Technology**

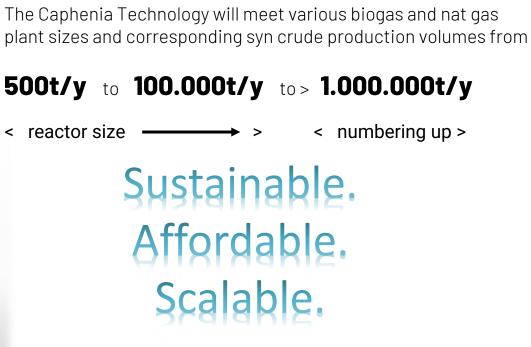
Most of the existing biogas plants can be upgraded – new ones optimized



## The Caphenia Route: One Technology fits All

Decentral medium - to semi central and central large





### What does CAPHENIA's PBtL/PGtL do better than e-fuel processes?

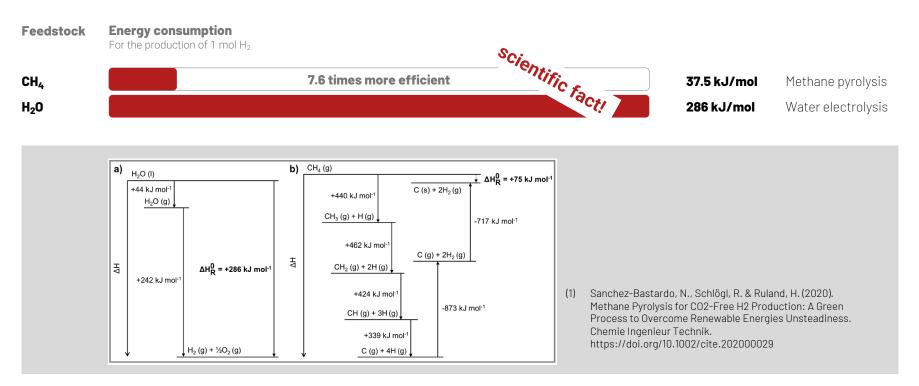
A real competive edge

### Significantly less demand of renewable electricity



## The extraction of $H_2$ from methane is highly energy-efficient

Methane pyrolysis represents a valuable alternative to water electrolysis



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### The Core Technology: The Plasma Boudouard Reactor

First kind of its art



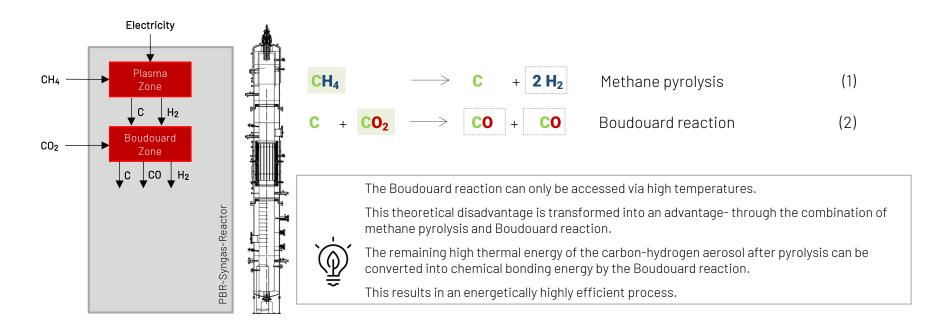
### CAPHENIA uses methane pyrolysis for $H_2$ production

Three quarters of the hydrogen in the novel synthesis gas process results from the pyrolysis of methane



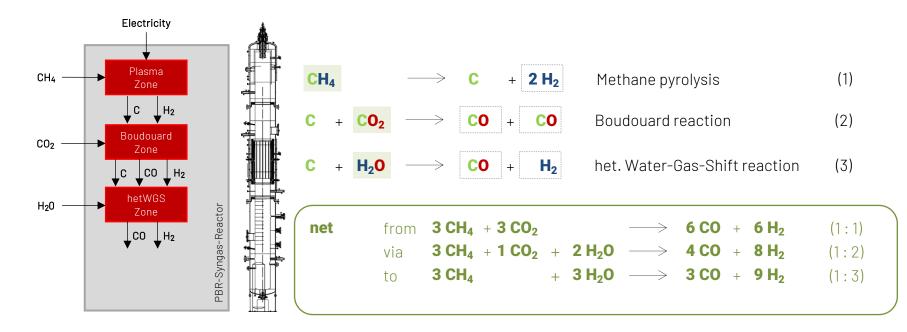
## **CAPHENIA** combines methane pyrolysis with Boudouard

Thereby disadvantages of the individual processes are transformed into an overall systemic advantage



### CAPHENIA combines hetWGS and creates a novel flexible syngas process

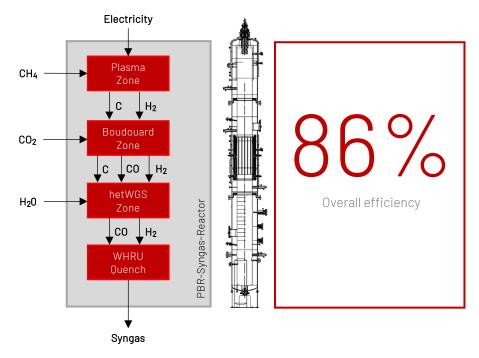
The CO:H<sub>2</sub> ratio inside the synthesis gas is adjustable



The het. water gas shift reaction allows the exact adjustment of the molecule ratio between CO and H2. For the purpose of a Fischer Tropsch Synthesis ( > fuels and chem. Bulk) and a Methane Synthesis ( Mathane > fuels and chem. bulk) a 1:2 ratio is required

## Heat recovery makes the CAPHENIA-process additionally efficient

Quench prevents back reactions



#### **Heat recovery**

After passing through the hetWGS-stage, the synthesis gas still has a temperature of approx. 900°C. This thermal energy is recovered via heat exchangers and used to preheat the feedstock gases ( $CH_4$ ,  $CO_2$  und  $H_2O$ ). Thus the overall process achieves an efficiency<sup>(1)</sup> of 86%.

#### Quench

The last process step includes a so-called quench. Here the synthesis gas is cooled down in a short time window in order to quickly transit the temperature range in which back reactions (e.g. methanation) can take place. This rapid cooling prevents the back reactions.

#### **PBR-Syngas Reactor**

All process steps take place in a single reactor in different zones.

hetWGS heterogene Wasser-Gas-Shift PBR Plasma-Boudouard-Reactor

(1) Efficiency is defined by the ratio of energy output (thermal, chemical) to energy input (electrical, thermal, chemical)

### **CAPHENIA's PBR\* Technology based on Biomass/Biogas**

There is no better match

### A Bioenergy Circular Economy

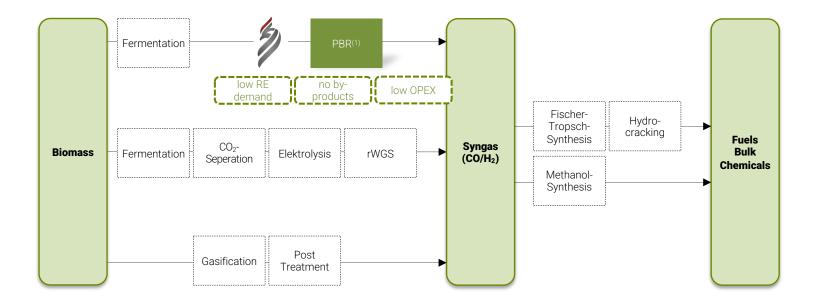
circulate products and materials at their highest value



\* Plasma Boudouard Reactor

### Main Routes from Biomass to Syn Gas to Fuel/Chem Bulk

Classification of the Power-and-Biogas-to-Liquid-Route



## Caphenia offers a competitive Package

Maturing markets will decide

Cost driversPrice of feedstock accounts for majority of production costRefining ethanol into jet fuel presents biggest cost bucket Both steps (ethanol ac acpex-intensive with ad cline potential in refining duction and jet production ostGasification-FT production cost is largely driven by capital costCosts for both RWGS and SOEC routes are highly driven by cost of electricity either for hydrogen production or co-electrolysisCost(green) H, presents the biggest opportunity for HEFA production costLimited supply of feedstock reductionOpex of refining step likely remains relatively highCapex to build gasifier remains high even after an expected strong decline between 2025 and 2030Despite steep decline, cost of green electricity remains strong decline between 2025 and 2030Despite steep decline, cost of green electricity remains capex only limited reduction potential	for majority of production cost and is market-driven based on scarceness of feedstock. Cost of (green) H <sub>2</sub> presents the biggest opportunity for HEFA production cost improvement   presents biggest cost bucket Both steps (ethanol are capex-intensive with decline potential in refining due to learning effects   cost is largely driven by capital cost   SOEC routes are highly driven by cost of electricity either for hydrogen production or co-electrolysis     Cost reduction constraints   Limited supply of feedstock and high hurdles for expand- ing feedstock base to purposely grown oil energy plants constraints feedstock cost reduction   Opex of refining step likely remains relatively little additional potential   Capex to build gasifier remains high even after an expected strong decline between 2025 and 2030   Despite steep decline, cost of green electricity remains substantial Capex for FT+FWGS and FT+SOEC have only limited reduction potential     Clean Skies for Tomorrow: Sustainable Aviation Fuels as a Pathway to Net-Zero Aviation		Pathway	HEFA	Alcohol-to-jet	Gasification/	Power-to-liquid	
reduction constraints and high hurdles for expand- ing feedstock base to purposely grown oil energy plants constraints feedstock remains relatively high Ethanol production capex already realized learning rate effects, resulting in relatively high even after an expected strong decline between 2025 already realized learning rate 2005 green electricity remains substantial	reduction constraints   and high hurdles for expand- ing feedstock base to purposely grown oil energy plants constrains feedstock cost reduction   remains relatively high Ethanol production capex and region relatively high thanol production capex and 2030   high even after an expected strong decline between 2025 and 2030   green electricity remains substantial     Clean Skies for Tomorrow:   Sustainable Aviation Fuels as a Pathway to Net-Zero Aviation		Cost drivers	for majority of production cost and is market-driven based on scarceness of feedstock Cost of (green) H <sub>2</sub> presents the biggest opportunity for HEFA production cost	presents biggest cost bucket Both steps (ethanol production and jet production) are capex-intensive with decline potential in refining	cost is largely driven by	SOEC routes are highly driven by cost of electricity either for hydrogen production or co-electrolysis Both PL routes are also capex-intensive and depend-	
			reduction	and high hurdles for expand- ing feedstock base to purposely grown oil energy plants constrains feedstock	remains relatively high Ethanol production capex already realized learning rate effects, resulting in relatively	high even after an expected strong decline between 2025	green electricity remains substantial Capex for FT+RWGS and FT+SOEC have only limited	
Clean Skies for Tomorrow: Sustainable Avlation Fuels as a Pathway to Net-Zero Avlation					Clean Skies for Tomo	prrow: Sustainable Aviation Fuels as a	Pathway to Net-Zero Aviation	
Solution : CARHENIA Power-and-Biomass-to-Liquid (PBtL) Power-and-(nat) Gas-		Wide biogenic feedstock base Besides fats and oils, additional so-called advanced biomasses can be used: urban waste,		no by-	ate production co products	up to 92% CO <sub>2</sub> - reduction	Low proc	duction cos

agricultural waste. Sewage sludge, etc. Mega natural gas feedstock base

CO2 reduction 25-92\*%, billion tons production possible

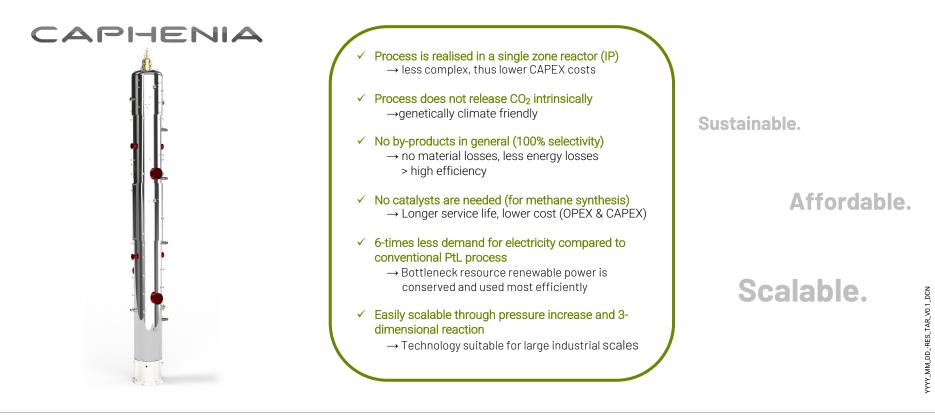


\*TUHH (Technical University Hamburg-Harburg) Life Cycle Analysis

1) CAPHENIA (2020). Own calculations based on MAN Engineering

### **CAPHENIA's Power & Biogas to Liquid Process**

The Highlights – Executive Summary



## **Outlook : CO<sub>2</sub> negative Hydrogene**

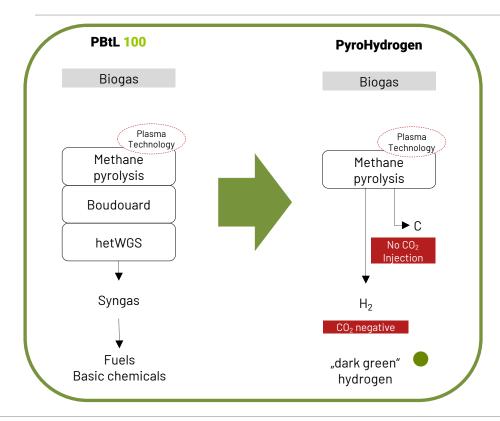
Based on same Caphenia core technology

### Since the World will not become CO2 neutral in all sectors – We need to become CO2 negative wherever we can!



### One more Option for decarbonising transport and industry

CAPHENIA develops key technology based on own IP for CO<sub>2</sub> NEGATIVE H<sub>2</sub> production





- 100% subsidary of Caphenia
- CO2 negative H2 production
- will become operative 2025ff

### The Know How Difference

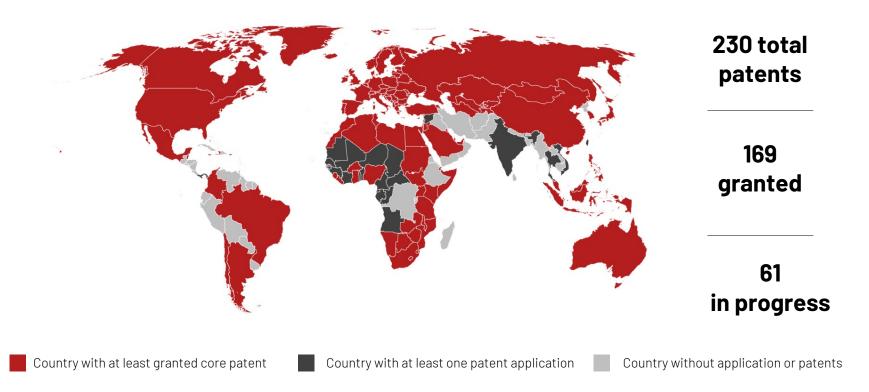
Competition yes - but not based on the same technology

### Caphenia is the sole owner of its Intellectual Property



## **Global IP protection**

The CAPHENIA process is patent protected in all relevant global markets



CAPHENIA

22

### 2023: A first of its kind plant will be build

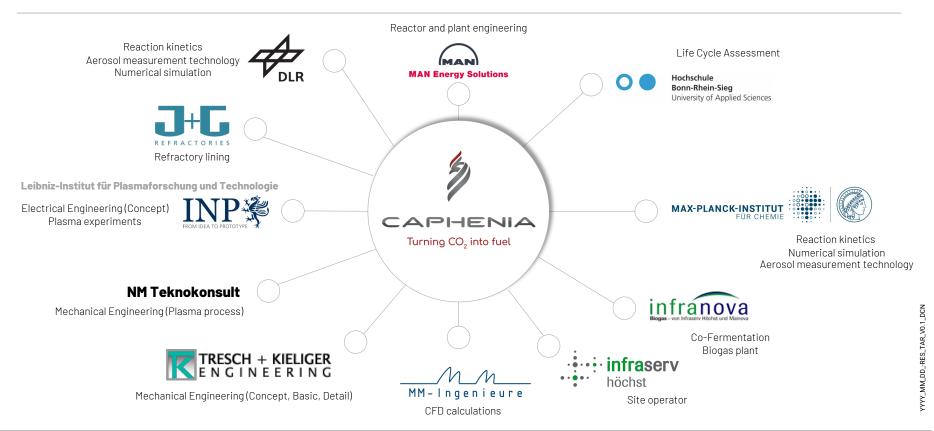
Pilot plant will be upgraded to demonstrator size until 2026

### Pilot Plant at Industry Park Infraserve, Frankfurt/Germany



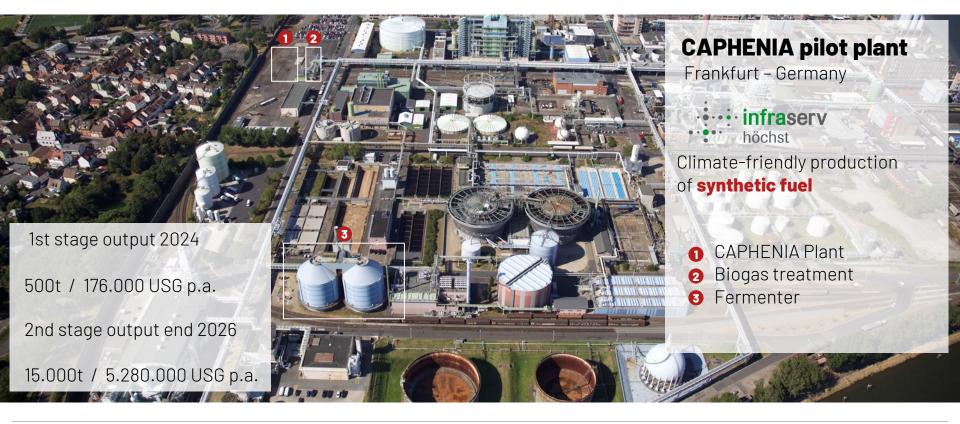
### The current development partnerships

CAPHENIA orchestrates a strong team



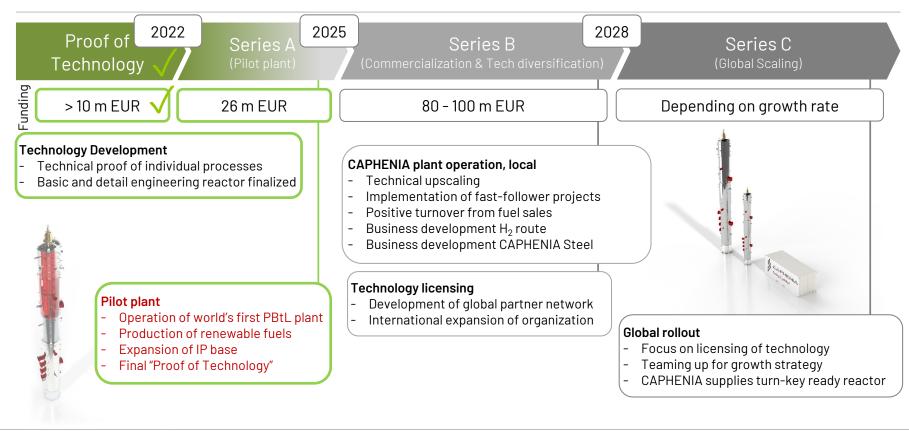
### Location of the Caphenia pilot plant: Frankfurt - Germany

Start construction of components Q2 2023 - Start operation Q1 2025



### The commercialization strategy

Rapid market entry. Expansion of the product portfolio. Global rollout through technology licensing.



# Sustainable Affordable Scalable



# Thank you!

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www.CAPHENIA.com